

Stellenbosch

South Africa

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"Ways forward to promote resources equity: The role of cleaner production and circular economy as moderator. Action or Reaction to Save the Planet"

INTERNATIONAL WORKSHOP ON ADVANCES IN CLEANER PRODUCTION

#### **Oral Presentation**

**Recovery of Rare Earth Elements** from NdFeB Waste Magnets DURSKI, M., MANILAL, N., NAIDOO, P., MOODLEY, K



Marcin Durski **University of** KwaZulu-Natal



## Estimated increase in demand for REEs

12 (J) IWACP

By 2030, more than 50% of rare-earth elements, 55% of cobalt, and 36% of nickel will be consumed by BEVs and the associated charging infrastructure <sup>[2]</sup>



Estimated demand increase for critical minerals according to McKinsey<sup>[2]</sup>

<sup>[2]</sup> The net-zero materials transition: Implications for global supply chains; McKinsey on Risk,October 2022



#### **Global Production of REEs**



<sup>[1]</sup> Mineral commodity summaries 2022, U.S. Geological Survey



## **Environmental concerns**

- Soil erosion
- Acidic effluents from mines
- Heavy metals pollution of bodies of water
- Decrease of biodiversity
- GHG emissions



• Negative impact on human health

Photo by Omid Roshan

# Waste Permanent Magnets (WPM) recycling



EUROPEAN WPM RECYCLING PLANTS<sup>[3]</sup>

- STENA Recycling (Sweden) 6 tonnes of NdFeB powders per annum
- University of Birmingham (UK) 50 tonnes of NdFeB powders per annum
- Magneti Ljubljana (Slovenia) 50 tonnes of NdFeB powders per annum
- MIMplus Technologies (Germany) 10 tonnes of NdFeB powders per annum













#### Each experiment was conducted using Ig of WPM powder in 50ml of acid



# Leaching – Nd<sup>3+</sup> results



Nd<sup>3+</sup> ions concentration in leachate after leaching experiments with HNO<sub>3</sub>; Particle size (filled markers - 100 - 150µm; open markers - 600 µm): • – 45°C in 6.7M acid,  $\blacksquare$  – 60°C in 6.7M acid,  $\blacklozenge$  – 45°C in 12.3M acid,  $\blacktriangle$  – 60°C in 12.3M acid



# Leaching – Fe<sup>3+</sup> results



Fe<sup>3+</sup> ions concentration in leachate after leaching experiments with HNO<sub>3</sub>; Particle size (filled markers -100 - 150µm; open markers - 600 µm): • – 45°C in 6.7M acid,  $\blacksquare$  – 60°C in 6.7M acid,  $\blacklozenge$  – 45°C in 12.3M acid,  $\blacktriangle$  – 60°C in 12.3M acid







#### Extraction – Nd<sup>3+</sup> results



Distribution of Nd<sup>3+</sup> ions in extraction experiments using HDEHP in n-dodecane; • – 0.5M HDEHP (10 ml), • – IM HDEHP (10 ml),  $\circ$  - 0.5M HDEHP (100 ml),  $\Box$  – IM HDEHP (100 ml).



#### Extraction – Fe<sup>3+</sup> results



Distribution of Fe<sup>3+</sup> ions in extraction experiments using HDEHP in n-dodecane; • – 0.5M HDEHP (10 ml), • – IM HDEHP (10 ml),  $\circ$  - 0.5M HDEHP (100 ml),  $\Box$  – IM HDEHP (100 ml).



#### Extraction – results

Recovery of Nd<sup>3+</sup> and Fe<sup>3+</sup> ions at a given HDEHP concentration

lon	Scale	[HDEHP]/M	Recovery/%
Nd <sup>3+</sup>	Small scale		77.82 – 99.99
		0.5	73.00 – 79.42
	Large scale	I	65.21 – 86.68
		0.5	62.33 – 70.95
Fe <sup>3+</sup>	Small scale	l	1.23 – 1.89
		0.5	3.52 – 8.02
	Large scale	I	0.69 – 1.23
		0.5	3.09 – 6.68







## Precipitation

Recovery of Nd<sup>3+</sup> ions obtained after precipitation processes at a given HDEHP concentration (M) and various oxalic acid (OA) to organic phase (OP) volume ratios.

[HDEHP]/M	OA:OP ratio	Recovery of Nd <sup>3+</sup> /%	
	1:1	71.18 ± 0.10	
	2:1	90.86 ± 0.23	
0.5	5:1	95.54 ± 0.12	
	10:1	96.37 ± 0.13	
	1:1	70.43 ± 0.11	
1	2:1	90.59 ± 0.34	
<b>–</b>	5:1	95.39 ± 0.22	
	10:1	97.22 ± 0.09	



#### Conclusions

- Optimal leaching conditions: 100-150  $\mu$ m & 12.3M HNO<sub>3</sub> at 60°C for 24 hours.
- HDEHP was proven a good extractant.
- Precipitation with saturated oxalic acid solution showed > 95% recovery of Nd<sup>3+</sup> ions using precipitant-to-extractant ratios above 5:1.
- Upscaling of the process is possible.



# THANK YOU





# Hydrometallurgy – chemistry of the process

Ranges of concentrations of elements in NdFeB magnets <sup>[4,5,6]</sup>

Fe <sup>3+</sup>	Nd <sup>3+</sup>	Dy <sup>3+</sup>	Pr <sup>3+</sup>	B <sup>3+</sup>	Sm <sup>3+</sup>
~59-69%	~22-33%	~0.5-5%	~ -7%	~I-2.5%	~0.6-1.6%

$$RE + 3H^+X^-_{(aq)} \rightarrow RE^{3+}_{(aq)} + 3X^-_{(aq)} + 1.5H_{2(g)}$$

$$RE^{3+}_{(aq)} + 3H^+Y^-_{(org)} \to RE^{3+}Y^-_{3(org)} + H^+_{(aq)}$$

$$2RE^{3+}Y_{3(org)}^{-} + 3C_{2}H_{2}O_{4(aq)} \rightarrow RE_{2}^{3+}(C_{2}O_{4})_{3(aq)}^{2-} + 6H^{+}Y_{(org)}^{-}$$

[4] Gruber, V., & Carsky, M. (2020). South African J. Chem. Eng., 33, 35–38.
[5] Lee, C.-H., Chen, Y.-J., Liao, C.-H., Popuri, S. R., Tsai, S.-L., & Hung, C.-E. (2013), Metall Mater Trans A, 44(13), 5825–5833.
[6] Reisdörfer, G., Bertuol, D., & Tanabe, E. H. (2019). Minerals Eng., 143, 105938.